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(54) Title: TETRAMERIZATION OF OLEFINS

(57) Abstract: The invention describes a process for tetramerisation of olefins wherein the product stream of the process contains more than 30% of the tetramer olefin. The process includes the step of contacting an olefinic feedstream with a catalyst system containing a transition metal compound and a heteroatomic ligand.

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TETRAMERIZATION OF OLEFINS

Field of the invention:

This invention relates to the oligomerisation of ethylene. More particularly, the invention relates to a tetramerisation process, a catalyst system for tetramerisation of olefins and the identification and use of ligands for a catalyst system for tetramerisation of olefins.

Background of the invention

This invention defines a process and catalyst system, that facilitates the production of 1-octene in high selectivity, while avoiding the co-production of significant quantities of butenes, other octene isomers, specific higher oligomers and polyethylene. The catalyst system can also be used for the tetramerisation of other olefins, especially α -olefins.

Despite the well known value of 1-octene, the art does not teach a commercially successful process for the tetramerisation of ethylene to produce 1-octene selectively. Conventional ethylene oligomerisation technologies produce a range of α olefins following either a Schulz-Flory or Poisson product distribution. By definition, these mathematical distributions limit the mass % of the tetramer that can be formed and make a distribution of products. In this regard, it is known from the prior art (US patent 6,184,428) that a nickel catalyst comprising a chelating ligand, preferably 2-diphenyl phosphino benzoic acid (DPPBA), a nickel compound, preferably $\text{NiCl}_2 \cdot 6\text{H}_2\text{O}$, and a catalyst activator, preferably sodium tetraphenylborate, catalyse the oligomerisation of ethylene to yield a mixture of linear olefins. The selectivity towards linear C8 α -olefins is claimed to be 19%. Similarly the Shell Higher Olefins Process (SHOP process, US patents 3,676,523 and 3,635,937) using a similar catalyst system is reported to typically yield 11 mass % 1-octene in its product mixture (Chem Systems PERP reports 90-1, 93-6 and 94/95S12).

Ziegler-type technologies based on trialkylaluminium catalysts, independently developed by Gulf Oil Chemicals Company (Chevron, e.g. DE patent 1,443,927) and Ethyl Corporation (BP/Amoco, e.g. US patent 3,906,053), are also commercially used to

oligomerise ethylene to mixtures of olefins that reportedly contain 13-25 mass % 1-octene (Chem Systems PERP reports 90-1, 93-6, and 94/95S12).

The prior art also teaches that chromium-based catalysts containing heteroatomic ligands with both phosphorus and nitrogen heteroatoms selectively catalyse the trimerisation of ethylene to 1-hexene. Examples of such heteroatomic ligands for ethylene trimerisation include bis(2-diethylphosphino-ethyl) amine (WO 03/053891, hereby fully incorporated herein by means of reference) as well as (o-methoxyphenyl)₂PN(methyl)P(o-methoxyphenyl)₂ (WO 02/04119, hereby fully incorporated herein by means of reference). Both these catalyst systems and processes are very specific for the production of 1-hexene and only yield 1-octene as an impurity (typically less than 3 mass % of the product mixture as disclosed by WO 02/04119). The coordinating phosphorus heteroatoms in (o-methoxyphenyl)₂PN(methyl)P(o-methoxyphenyl)₂ (WO 02/04119) are spaced apart by one nitrogen atom. It is believed that the nitrogen atom does not coordinate, at least in the absence of an activator, with the chromium and that without any further electron donating atoms on the ligand that it is a bidentate system. Furthermore it is argued that the polar, or electron donating substituents in the ortho-position of the phenyl groups help form a tridentate system, which is generally believed to enhance selectivity towards 1-hexene formation as reiterated by the inventor of WO 02/04119 in *Chem. Commun.*, 2002, 858-859 by stating "This has led us to hypothesise that the potential for ortho-methoxy groups to act as pendent donors and increase the coordinative saturation of the chromium centre is an important factor." To support their hypothesis, the authors of *Chem. Commun.*, 2002, 858-859 showed that the use of (p-methoxyphenyl)₂PN(methyl)P(p-methoxyphenyl)₂, a compound without any such ortho-polar substituents on at least one of R¹, R², R³ and R⁴, as a ligand under catalytic conditions resulted in no catalytic activity towards α -olefins. WO 02/04119 (Example 16) teaches the production of octenes using a trimerisation of olefins process and catalyst system. In this instance, 1-butene was co-trimerised with two ethylene molecules to give 25% octenes. However, the nature of these octenes was not disclosed and the applicant believes that they consist of a mixture of linear and branched octenes.

The prior art teaches that high 1-octene selectivities cannot be achieved since expansion of the generally accepted seven-membered metallacycle reaction

intermediate for ethylene trimerisation (*Chem. Commun.*, 1989, 674) to a nine-membered metallacycle is unlikely to occur (*Organometallics*, 2003, 22, 2564; *Angew. Chem. Int. Ed.*, 2003, 42 (7), 808). It is argued that the nine-membered ring is the least favoured medium sized ring and should thus be disfavoured relative to the seven-membered ring (*Organometallics*, 2003, 22, 2564). In addition, it is also stated by the same authors that, "if a nine-membered ring formed, it would be more likely to grow to an eleven- or thirteen-membered ring...In other words, one would never expect much octene, but formation of some (linear) decene or dodecene would be more reasonable."

Despite the teaching of the opposite, the applicant has now found a process for selectively producing a tetramerised olefin. The applicant has further found that chromium-based catalysts containing mixed heteroatomic ligands with both nitrogen and phosphorus heteroatoms, with polar substituents on the hydrocarbyl or heterohydrocarbyl groups on the phosphorous atoms, can be used to selectively tetramerise ethylene to 1-octene often in excess of 60 mass% selectivity. This high 1-octene selectivity cannot be achieved *via* conventional one-step ethylene oligomerisation or trimerisation technologies which at most yield 25 mass% 1-octene.

Summary of the invention

This invention relates to a process for selectively producing tetrameric products.

This invention specifically relates to a process for selectively producing tetrameric products such as 1-octene from olefins such as ethylene.

The invention relates to a process of selectively producing tetrametric products using a transition metal catalyst system containing a heteroatomic ligand.

According to a first aspect of the invention there is provided a process for tetramerisation of olefins wherein the product of the tetramerisation process is an olefin and makes up more than 30% of the product stream of the process.

According to a second aspect of the invention the tetramerisation process includes the step of contacting an olefinic feedstream with a catalyst system which includes a

transition metal and a heteroatomic ligand and wherein the product of the tetramerisation process is an olefin and makes up more than 30% of the product stream of the process.

In this specification, % will be understood to be a mass %.

The term "tetramerisation" generally refers to the reaction of four, and preferably four identical, olefinic monomer units to yield a linear and/or branched olefin.

By heteroatomic is meant a ligand that contains at least two heteroatoms, which can be the same or different, where the heteroatoms may be selected from phosphorus, arsenic, antimony, sulphur, oxygen, bismuth, selenium or nitrogen.

The feedstream will be understood to include an olefin to be tetramerised and can be introduced into the process according to the invention in a continuous or batch fashion.

The product stream will be understood to include a tetramer, which tetramer is produced according to the invention in a continuous or batch fashion.

The feedstream may include an α -olefin and the product stream may include at least 30%, preferably at least 35%, of a tetramerised α -olefin monomer.

The process may include a process for tetramerisation of α -olefins. Under the term α -olefins is meant all hydrocarbon compounds with terminal double bonds. This definition includes ethylene, propylene, 1-butene, isobutylene, 1-pentene, 1-hexene, 1-octene and the like.

The process may include a process for tetramerisation of α -olefins to selectively yield tetrameric α -olefin products.

The olefinic feedstream may include ethylene and the product stream may include at least 30% 1-octene. The process may be a process for tetramerisation of ethylene.

The invention allows the ligand, catalyst system and/or process conditions to be selected to give a product stream of more than 40%, 50%, or 60% α -olefins. It may be

preferable, depending on the further use of the product stream, to have such high selectivities of the α -olefin.

The olefinic feedstream may include ethylene and the $(C_6 + C_8) : (C_4 + C_{10})$ ratio in the product stream may be more than 2.5:1.

The olefinic feedstream may include ethylene and the $C_8 : C_6$ ratio in the product stream is more than 1.

The ethylene may be contacted with the catalyst system at a pressure of greater than 1 barg and preferably greater than 10 barg, more preferably greater than 30 barg.

The heteroatomic ligand may be described by the following general formula $(R)_nA-B-C(R)_m$ where A and C are independently selected from a group which comprises phosphorus, arsenic, antimony, oxygen, bismuth, sulphur, selenium, and nitrogen, and B is a linking group between A and C, and R is independently selected from any homo or heterohydrocarbyl group of which at least one R group is substituted with a polar substituent and n and m is determined by the respective valence and oxidation state of A and C.

A and/or C may be a potential electron donor for coordination with the transition metal.

An electron donor or electron donating substituent is defined as that entity that donates electrons used in chemical, including dative covalent, bond formation.

The heteroatomic ligand may be described by the following general formula $(R^1)(R^2)A-B-C(R^3)(R^4)$ where A and C are independently selected from a group which comprises phosphorus, arsenic, antimony, bismuth and nitrogen and B is a linking group between A and C, and R^1 , R^2 , R^3 and R^4 are independently selected from non-aromatic and aromatic, including heteroaromatic, groups of which at least one of R^1 , R^2 , R^3 and R^4 is substituted with a polar substituent.

In some embodiments of the process aspect of the invention, up to four of R^1 , R^2 , R^3 and R^4 may have substituents on the atom adjacent to the atom bound to A or C.

In addition to at least one of R^1 , R^2 , R^3 and R^4 being substituted with a polar substituent, each of R^1 , R^2 , R^3 and R^4 may be aromatic, including heteroaromatic, but preferably not all of R^1 , R^2 , R^3 and R^4 , if they all are aromatic, are substituted by any substituent on an atom adjacent to the atom bound to A or C.

In addition to at least one of R^1 , R^2 , R^3 and R^4 being substituted with a polar substituent, not more than two of R^1 , R^2 , R^3 and R^4 , if they are aromatic, may have substituents on the atom adjacent to the atom bound to A or C.

Any polar substituents on R^1 , R^2 , R^3 and R^4 , if they are aromatic, may preferably not be on the atom adjacent to the atom bound to A or C.

At least one of R^1 , R^2 , R^3 and R^4 , if aromatic, may be substituted with a polar substituent on the 2nd or further atom from the atom bound to A or C.

Any polar substituent on one or more of R^1 , R^2 , R^3 and R^4 may be electron donating.

Polar is defined by IUPAC as an entity with a permanent electric dipole moment. Polar substituents include methoxy, ethoxy, isopropoxy, C_3 - C_{20} alkoxy, phenoxy, pentafluorophenoxy, trimethylsiloxy, dimethylamino, methylsulfanyl, tosyl, methoxymethyl, methylthiomethyl, 1,3-oxazolyl, methomethoxy, hydroxyl, amino, phosphino, arsino, stibino, sulphate, nitro and the like.

Any of the groups R^1 , R^2 , R^3 and R^4 may independently be linked to one or more of each other or to the linking group B to form a cyclic structure together with A and C, A and B or B and C.

R^1 , R^2 , R^3 and R^4 may be independently selected from a group comprising a benzyl, phenyl, tolyl, xylyl, mesityl, biphenyl, naphthyl, anthracenyl, methoxy, ethoxy, phenoxy, tolyloxy, dimethylamino, diethylamino, methylethylamino, thiophenyl, pyridyl, thioethyl, thiophenoxy, trimethylsilyl, dimethylhydrazyl, methyl, ethyl, ethenyl, propyl, butyl, propenyl, propynyl, cyclopentyl, cyclohexyl, ferrocenyl and tetrahydrofuranyl group.

Preferably, R^1 , R^2 , R^3 and R^4 may independently be selected from a group comprising a phenyl, tolyl, biphenyl, naphthyl, thiophenyl and ethyl group.

A and/or C may be independently oxidised by S, Se, N or O, where the valence of A and/or C allows for such oxidation.

A and C may be independently phosphorus or phosphorus oxidised by S or Se or N or O.

B may be selected from any one of a group comprising: organic linking groups comprising a hydrocarbyl, substituted hydrocarbyl, heterohydrocarbyl and a substituted heterohydrocarbyl; inorganic linking groups comprising single atom links; ionic links; and a group comprising methylene, dimethylmethylene, 1,2-ethane, 1,2-phenylene, 1,2-propane, 1,2-catechol, 1,2-dimethylhydrazine, $-B(R^5)-$, $-Si(R^5)_2-$, $-P(R^5)-$ and $-N(R^5)-$ where R^5 is hydrogen, a hydrocarbyl or substituted hydrocarbyl, a substituted heteroatom or a halogen. Preferably, B may be $-N(R^5)-$ and R^5 is a hydrocarbyl or a substituted hydrocarbyl group. R^5 may be hydrogen or may be selected from the groups consisting of alkyl, substituted alkyl, aryl, substituted aryl, aryloxy, substituted aryloxy, halogen, nitro, alkoxycarbonyl, carbonyloxy, alkoxy, aminocarbonyl, carbonylamino, dialkylamino, silyl groups or derivatives thereof, and aryl substituted with any of these substituents. Preferably R^5 may be an isopropyl, a 1-cyclohexylethyl, a 2-methylcyclohexyl or a 2-octyl group.

B may be selected to be a single atom spacer. A single atom linking spacer is defined as a substituted or non-substituted atom that is bound directly to A and C.

The ligand may also contain multiple $(R)_nA-B-C(R)_m$ units. Non limiting examples of such ligands include dendrimeric ligands as well as ligands where the individual units are coupled either *via* one or more of the R groups or *via* the linking group B. More specific, but non limiting, examples of such ligands may include 1,2-di-(N(P(4-methoxyphenyl)₂)₂)-benzene, 1,4-di-(N(P(4-methoxyphenyl)₂)₂)-benzene, N(CH₂CH₂N(P(4-methoxyphenyl)₂)₂)₃ and 1,4-di-(P(4-methoxyphenyl)N(methyl)P(4-methoxyphenyl)₂)-benzene.

The ligands can be prepared using procedures known to one skilled in the art and procedures disclosed in published literature. Examples of ligands are: (3-methoxyphenyl)₂PN(methyl)P(3-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(methyl)P(4-methoxyphenyl)₂, (3-methoxyphenyl)₂PN(isopropyl)P(3-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(2-ethylhexyl)P(4-methoxyphenyl)₂, (3-methoxyphenyl)(phenyl)PN(methyl)P(phenyl)₂ and (4-methoxyphenyl)(phenyl)PN(methyl)P(phenyl)₂, (3-methoxyphenyl)(phenyl)PN(methyl)P(3-methoxyphenyl)(phenyl), (4-methoxyphenyl)(phenyl)PN(methyl)P(4-methoxyphenyl)(phenyl), (3-methoxyphenyl)₂PN(methyl)P(phenyl)₂ and (4-methoxyphenyl)₂PN(methyl)P(phenyl)₂, (4-methoxyphenyl)₂PN(1-cyclohexylethyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(2-methylcyclohexyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(decyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(pentyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(benzyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(phenyl)P(4-methoxyphenyl)₂, (4-fluorophenyl)₂PN(methyl)P(4-fluorophenyl)₂, (2-fluorophenyl)₂PN(methyl)P(2-fluorophenyl)₂, (4-dimethylamino-phenyl)₂PN(methyl)P(4-dimethylamino-phenyl)₂, (4-methoxyphenyl)₂PN(allyl)P(4-methoxyphenyl)₂, (phenyl)₂PN(isopropyl)P(2-methoxyphenyl)₂, (4-(4-methoxyphenyl)-phenyl)₂PN(isopropyl)P(4-(4-methoxyphenyl)-phenyl)₂ and (4-methoxyphenyl)(phenyl)PN(isopropyl)P(phenyl)₂.

The catalyst system may include an activator and the process may include the step of combining in any order a heteroatomic ligand with a transition metal compound and an activator.

The process may include the step of generating a heteroatomic coordination complex *in situ* from a transition metal compound and a heteroatomic ligand. The process may include the step of adding a pre-formed coordination complex, prepared using a heteroatomic ligand and a transition metal compound, to a reaction mixture, or the step of adding separately to the reactor, a heteroatomic ligand and a transition metal compound such that a heteroatomic coordination complex of a transition metal is generated *in situ*. By generating a heteroatomic coordination complex *in situ* is meant that the complex is generated in the medium in which catalysis takes place. Typically, the heteroatomic coordination complex is generated *in situ*. Typically, the transition

metal compound, and heteroatomic ligand are combined (both *in situ* and *ex situ*) to provide metal/ligand ratios from about 0.01:100 to 10 000:1, and preferably, from about 0.1:1 to 10:1.

The transition metal may be selected from any one of a group comprising chromium, molybdenum, tungsten, titanium, tantalum, vanadium and zirconium, preferably chromium.

The transition metal compound which, upon mixing with the heteroatomic ligand and an activator, catalyses ethylene tetramerisation in accordance with the invention, may be a simple inorganic or organic salt, a co-ordination or organometallic complex and may be selected from any one of a group comprising chromium trichloride tris-tetrahydrofuran complex, (benzene)tricarbonyl chromium, chromium (III) octanoate, chromium hexacarbonyl, chromium (III) acetylacetonate and chromium (III) 2-ethylhexanoate. The preferred transition metal compounds include chromium (III) acetylacetonate and chromium (III) 2-ethylhexanoate.

The heteroatomic ligand can be modified to be attached to a polymer chain so that the resulting heteroatomic coordination complex of the transition metal is soluble at elevated temperatures, but becomes insoluble at 25°C. This approach would enable the recovery of the complex from the reaction mixture for reuse and has been used for other catalyst as described by D.E. Bergbreiter *et al.*, *J. Am. Chem. Soc.*, 1987, **109**, 177-179. In a similar vein these transition metal complexes can also be immobilised by binding the heteroatomic ligands for example to silica, silica gel, polysiloxane, alumina backbone or the like as demonstrated, for example, by C. Yuanyin *et al.*, *Chinese J. React. Pol.*, 1992, **1**(2), 152-159 for immobilising platinum complexes.

The activator for use in the process may in principle be any compound that generates an active catalyst when combined with the heteroatomic ligand and the transition metal compound. Mixtures of activators may also be used. Suitable compounds include organoaluminium compounds, organoboron compounds, organic salts, such as methyllithium and methylmagnesium bromide, inorganic acids and salts, such as tetrafluoroboric acid etherate, silver tetrafluoroborate, sodium hexafluoroantimonate and the like.

Suitable organoaluminium compounds include compounds of the formula AlR_3 , where each R is independently a C_1 - C_{12} alkyl, an oxygen containing moiety or a halide, and compounds such as $LiAlH_4$ and the like. Examples include trimethylaluminium (TMA), triethylaluminium (TEA), tri-isobutylaluminium (TIBA), tri-*n*-octylaluminium, methylaluminium dichloride, ethylaluminium dichloride, dimethylaluminium chloride, diethylaluminium chloride, aluminium isopropoxide, ethylaluminiumsesquichloride, methylaluminiumsesquichloride, and aluminoxanes. Aluminoxanes are well known in the art as typically oligomeric compounds which can be prepared by the controlled addition of water to an alkylaluminium compound, for example trimethylaluminium. Such compounds can be linear, cyclic, cages or mixtures thereof. Mixtures of different aluminoxanes may also be used in the process.

Examples of suitable organoboron compounds are boroxines, $NaBH_4$, triethylborane, tris(pentafluorophenyl)borane, tributyl borate and the like.

The activator may also be or contain a compound that acts as a reducing or oxidising agent, such as sodium or zinc metal and the like, or oxygen and the like.

The activator may be selected from alkylaluminoxanes such as methylaluminoxane (MAO) and ethylaluminoxane (EAO) as well as modified alkylaluminoxanes such as modified methylaluminoxane (MMAO). Modified methylaluminoxane (a commercial product from Akzo Nobel) contains modifier groups such as isobutyl or *n*-octyl groups, in addition to methyl groups.

The transition metal and the aluminoxane may be combined in proportions to provide Al/metal ratios from about 1:1 to 10 000:1, preferably from about 1:1 to 1000:1, and more preferably from 1:1 to 300:1.

The process may include the step of adding to the catalyst system a trialkylaluminium compound in amounts of between 0.01 to 1000 mol per mol of alkylaluminoxane.

It should be noted that aluminoxanes generally also contain considerable quantities of the corresponding trialkylaluminium compounds used in their preparation. The presence

of these trialkylaluminium compounds in aluminoxanes can be attributed to their incomplete hydrolysis with water. Any quantity of a trialkylaluminium compound quoted in this disclosure is additional to alkylaluminium compounds contained within the aluminoxanes.

The process may include the step of mixing the components of the catalyst system at any temperature between -20°C and 250°C in the presence of an olefin. The applicant has found that the presence of an olefin may stabilise the catalyst system.

The individual components of the catalyst system described herein may be combined simultaneously or sequentially in any order, and in the presence or absence of a solvent, in order to give an active catalyst. The mixing of the catalyst components can be conducted at any temperature between -20°C and 250°C. The presence of an olefin during the mixing of the catalyst components generally provides a protective effect which may result in improved catalyst performance. The preferred temperature range may be between 20°C and 100°C.

The catalyst system, in accordance with the invention, or its individual components, may also be immobilised by supporting it on a support material, for example, silica, alumina, MgCl₂, zirconia or mixtures thereof, or on a polymer, for example polyethylene, polypropylene, polystyrene, or poly(aminostyrene). The catalyst can be formed *in situ* in the presence of the support material, or the support can be pre-impregnated or premixed, simultaneously or sequentially, with one or more of the catalyst components. In some cases, the support material can also act as a component of the activator. This approach would also facilitate the recovery of the catalyst from the reaction mixture for reuse. The concept was, for example, successfully demonstrated with a chromium-based ethylene trimerisation catalyst by T. Monoi and Y. Sasaki, *J. Mol. Cat.A:Chem.*, 1987, **109**, 177-179. In some cases, the support can also act as a catalyst component, for example where such supports contain aluminoxane functionalities or where the support is capable of performing similar chemical functions as an aluminoxane, which is for instance the case with IOLATM (a commercial product from Grace Davison).

The reaction products or in other words olefin oligomers, as described herein, may be prepared using the disclosed catalyst system by homogeneous liquid phase reaction in

the presence or absence of an inert solvent, and/or by slurry reaction where the catalyst system is in a form that displays little or no solubility, and/or a two-phase liquid/liquid reaction, and/or a bulk phase reaction in which neat reagent and/or product olefins serve as the dominant medium, and/or gas phase reaction, using conventional equipment and contacting techniques.

The process may therefore also be carried out in an inert solvent. Any inert solvent that does not react with the activator can be used. These inert solvents may include any saturated aliphatic and unsaturated aliphatic and aromatic hydrocarbon and halogenated hydrocarbon. Typical solvents include, but are not limited to, benzene, toluene, xylene, cumene, heptane, methylcyclohexane, methylcyclopentane, cyclohexane, 1-hexene, 1-octene, ionic liquids and the like.

The process may be carried out at pressures from atmospheric to 500 barg. Ethylene pressures in the range of 10-70 barg are preferred. Particularly preferred pressures range from 30-50 barg.

The process may be carried out at temperatures from - 20 °C - 250 °C. Temperatures in the range of 15-130 °C are preferred. Particularly preferred temperatures range from 35-100°C.

In a preferred embodiment of the invention, the heteroatomic coordination complex and reaction conditions are selected such that the yield of 1-octene from ethylene is greater than 30 mass %, preferably greater than 35 mass %. In this regard yield refers to grams of 1-octene formed per 100g of total reaction product formed.

In addition to 1-octene, the process may also yield different quantities of 1-butene, 1-hexene, methylcyclopentane, methylene cyclopentane, propylcyclopentane, propylene cyclopentane and specific higher oligomers, depending on the nature of the heteroatomic ligand and the reaction conditions. A number of these products cannot be formed *via* conventional ethylene oligomerisation and trimerisation technologies in the yields observed in the present invention.

Although the catalyst, its individual components, reagents, solvents and reaction products are generally employed on a once-through basis, any of these materials can, and are indeed preferred to be recycled to some extent in order to minimise production costs.

The process may be carried out in a plant which includes any type of reactor. Examples of such reactors include, but are not limited to, batch reactors, semi-batch reactors and continuous reactors. The plant may include, in combination a) a reactor, b) at least one inlet line into this reactor for olefin reactant and the catalyst system, c) effluent lines from this reactor for oligomerisation reaction products, and d) at least one separator to separate the desired oligomerisation reaction products, wherein the catalyst system may include a heteroatomic coordination complex of a transition metal compound and an activator, as described herein.

In another embodiment of the process the reactor and a separator may be combined to facilitate the simultaneous formation of reaction products and separation of these compounds from the reactor. This process principle is commonly known as reactive distillation. When the catalyst system exhibits no solubility in the solvent or reaction products, and is fixed in the reactor so that it does not exit the reactor with the reactor product, solvent and unreacted olefin, the process principle is commonly known as catalytic distillation.

According to a further aspect of the invention, there is provided a catalyst system, as described above, for the tetramerisation of olefins. The catalyst system may include a heteroatomic ligand as described above and a transition metal. The catalyst system may also include an activator as described above.

The heteroatomic ligand may be described by the following general formula $(R)_nA-B-C(R)_m$ where A and C are independently selected from a group which comprises phosphorus, arsenic, antimony, oxygen, bismuth, sulphur, selenium, and nitrogen, and B is a linking group between A and C, and R is independently selected from any homo or heterohydrocarbyl group of which at least one R group is substituted with a polar substituent and n and m is determined by the respective valence and oxidation state of A and C.

A and/or C may be a potential electron donor for coordination with the transition metal.

An electron donor or electron donating substituent is defined as that entity that donates electrons used in chemical, including dative covalent, bond formation.

The heteroatomic ligand may be described by the following general formula $(R^1)(R^2)A-B-C(R^3)(R^4)$ where A and C are independently selected from a group which comprises phosphorus, arsenic, antimony, bismuth and nitrogen and B is a linking group between A and C, and R^1 , R^2 , R^3 and R^4 are independently selected from non-aromatic and aromatic, including heteroaromatic, groups of which at least one of R^1 , R^2 , R^3 and R^4 is substituted with a polar substituent.

In addition to at least one of R^1 , R^2 , R^3 and R^4 being substituted with a polar substituent, each of R^1 , R^2 , R^3 and R^4 may be aromatic, including heteroaromatic, but preferably not all of R^1 , R^2 , R^3 and R^4 , if they all are aromatic, are substituted by any substituent on an atom adjacent to the atom bound to A or C.

In addition to at least one of R^1 , R^2 , R^3 and R^4 being substituted with a polar substituent, not more than two of R^1 , R^2 , R^3 and R^4 , if they are aromatic, may have substituents on the atom adjacent to the atom bound to A or C.

Any polar substituents on R^1 , R^2 , R^3 and R^4 , if they are aromatic, may preferably not be on the atom adjacent to the atom bound to A or C.

Any polar substituent on one or more of R^1 , R^2 , R^3 and R^4 may be electron donating.

Polar is defined as an entity with a permanent electric dipole moment. Polar substituents include methoxy, ethoxy, isopropoxy, C_3 - C_{20} alkoxy, phenoxy, pentafluorophenoxy, trimethylsiloxy, dimethylamino, methylsulfanyl, tosyl, methoxymethyl, methylthiomethyl, 1,3-oxazolyl, methomethoxy, hydroxyl, amino, phosphino, arsino, stibino, sulphate, nitro and the like.

Any of the groups R^1 , R^2 , R^3 and R^4 may independently be linked to one or more of each other or to the linking group B to form a cyclic structure together with A and C, A and B or B and C.

R^1 , R^2 , R^3 and R^4 may be independently selected from a group comprising a benzyl, phenyl, tolyl, xylyl, mesityl, biphenyl, naphthyl, anthracenyl, methoxy, ethoxy, phenoxy, tolyloxy, dimethylamino, diethylamino, methylethylamino, thiophenyl, pyridyl, thioethyl, thiophenoxy, trimethylsilyl, dimethylhydrazyl, methyl, ethyl, ethenyl, propyl, butyl, propenyl, propynyl, cyclopentyl, cyclohexyl, ferrocenyl and tetrahydrofuranyl group. Preferably, R^1 , R^2 , R^3 and R^4 may independently be selected from a group comprising a phenyl, tolyl, biphenyl, naphthyl, thiophenyl and ethyl group.

A and/or C may be independently oxidised by S, Se, N or O, where the valence of A and/or C allows for such oxidation.

A and C may be independently phosphorus or phosphorus oxidised by S or Se or N or O.

B may be selected from any one of a group comprising: organic linking groups comprising a hydrocarbyl, substituted hydrocarbyl, heterohydrocarbyl and a substituted heterohydrocarbyl; inorganic linking groups comprising single atom links; ionic links; and a group comprising methylene, dimethylmethylene, 1,2-ethane, 1,2-phenylene, 1,2-propane, 1,2-catechol, 1,2-dimethylhydrazine, $-B(R^5)-$, $-Si(R^5)_2-$, $-P(R^5)-$ and $-N(R^5)-$ where R^5 is hydrogen, a hydrocarbyl or substituted hydrocarbyl, a substituted heteroatom or a halogen. Preferably, B may be $-N(R^5)-$ and R^5 is a hydrocarbyl or a substituted hydrocarbyl group. R^5 may be hydrogen or may be selected from the groups consisting of alkyl, substituted alkyl, aryl, substituted aryl, aryloxy, substituted aryloxy, halogen, nitro, alkoxycarbonyl, carbonyloxy, alkoxy, aminocarbonyl, carbonylamino, dialkylamino, silyl groups or derivatives thereof, and aryl substituted with any of these substituents. Preferably R^5 may be an isopropyl, a 1-cyclohexylethyl, a 2-methylcyclohexyl or a 2-octyl group.

B may be selected to be a single atom spacer. A single atom linking spacer is defined as a substituted or non-substituted atom that is bound directly to A and C.

The ligand may also contain multiple $(R)_nA-B-C(R)_m$ units. Not limiting examples of such ligands include dendrimeric ligands as well as ligands where the individual units are coupled either *via* one or more of the R groups or *via* the linking group B. More specific, but not limiting, examples of such ligands may include 1,2-di-(N(P(4-phenyl)₂)₂)-benzene, 1,4-di-(N(P(4-methoxyphenyl)₂)₂)-benzene, N(CH₂CH₂N(P(4-methoxyphenyl)₂)₂)₃ and 1,4-di-(P(4-methoxyphenyl)N(methyl)P(4-methoxyphenyl)₂)-benzene.

The ligands can be prepared using procedures known to one skilled in the art and procedures disclosed in published literature. Examples of ligands are: (3-methoxyphenyl)₂PN(methyl)P(3-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(methyl)P(4-methoxyphenyl)₂, (3-methoxyphenyl)₂PN(isopropyl)P(3-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(2-ethylhexyl)P(4-methoxyphenyl)₂, (3-methoxyphenyl)(phenyl)PN(methyl)P(phenyl)₂ and (4-methoxyphenyl)(phenyl)PN(methyl)P(phenyl)₂, (3-methoxyphenyl)(phenyl)PN(methyl)P(3-methoxyphenyl)(phenyl), (4-methoxyphenyl)(phenyl)PN(methyl)P(4-methoxyphenyl)(phenyl), (3-methoxyphenyl)₂PN(methyl)P(phenyl)₂ and (4-methoxyphenyl)₂PN(methyl)P(phenyl)₂, (4-methoxyphenyl)₂PN(1-cyclohexylethyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(2-methylcyclohexyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(decyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(pentyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(benzyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(phenyl)P(4-methoxyphenyl)₂, (4-fluorophenyl)₂PN(methyl)P(4-fluorophenyl)₂, (2-fluorophenyl)₂PN(methyl)P(2-fluorophenyl)₂, (4-dimethylamino-phenyl)₂PN(methyl)P(4-dimethylamino-phenyl)₂, (4-methoxyphenyl)₂PN(allyl)P(4-methoxyphenyl)₂, (phenyl)₂PN(isopropyl)P(2-methoxyphenyl)₂, (4-(4-methoxyphenyl)-phenyl)₂PN(isopropyl)P(4-(4-methoxyphenyl)-phenyl)₂ and (4-methoxyphenyl)(phenyl)PN(isopropyl)P(phenyl)₂.

The transition metal may be selected from any one of a group comprising chromium, molybdenum, tungsten, titanium, tantalum, vanadium and zirconium, preferably chromium.

The transition metal may be derived from a transition metal compound selected from a simple inorganic or organic salt, a co-ordination or organometallic complex, which may be selected from a group comprising chromium trichloride tris-tetrahydrofuran complex, (benzene)tricarbonyl chromium, chromium (III) octanoate, chromium (III) acetylacetonate, chromium hexacarbonyl, and chromium (III) 2-ethylhexanoate. The preferred transition metal compounds include chromium (III) acetylacetonate and chromium (III) 2-ethylhexanoate.

The transition metal compound and heteroatomic ligand may have metal/ligand ratios from about 0.01:100 to 10 000:1, preferably from about 0.1:1 to 10:1.

The catalyst system may also include an activator as described above.

The activator may in principle be any compound that generates an active catalyst when combined with the heteroatomic ligand and the transition metal compound. Mixtures of activators may also be used. Suitable compounds include organoaluminium compounds, organoboron compounds, organic salts, such as methyllithium and methylmagnesium bromide, inorganic acids and salts, such as tetrafluoroboric acid etherate, silver tetrafluoroborate, sodium hexafluoroantimonate and the like.

The activator may be selected from alkylaluminoxanes such as methylaluminoxane (MAO) and ethylaluminoxane (EAO) as well as modified alkylaluminoxanes such as modified methylaluminoxane (MMAO). Modified methylaluminoxane (a commercial product from Akzo Nobel) contains modifier groups such as isobutyl or n-octyl groups, in addition to methyl groups. The transition metal and the aluminoxane may be in such proportions relative to each other to provide Al/metal ratios from about 1:1 to 10 000:1, preferably from about 1:1 to 1000:1, and more preferably from 1:1 to 300:1.

The catalyst system may also include a trialkylaluminium compound in amounts of between 0.01 to 100 mol per mol of aluminoxane.

According to an even further aspect of the invention, there is provided a ligand, as described above, for a catalyst system, as described above, for the tetramerisation of olefins.

The invention also extends to the identification and use of ligands suitable for use in a tetramerisation of olefins process or catalyst system.

EXAMPLES OF PERFORMING THE INVENTION

The invention will now be described with reference to the following examples which are not in any way intended to limit the scope of the invention. The individual components of the examples may conceivably be omitted or substituted and, although not necessarily ideal, the invention may conceivably still be performed and these components are not to be taken as essential to the working of the invention.

In the examples that follow all procedures were carried out under inert conditions, using pre-dried reagents. Chemicals were obtained from Sigma-Aldrich or Strem Chemicals unless stated otherwise. All trialkylaluminium and aluminosilane compounds and solutions thereof were obtained from Crompton GmbH, Akzo Nobel and Albemarle Corporation. In all the examples, the molar mass of methylaluminosilane (MAO) was taken to be 58.016 g/mol, corresponding to the $(\text{CH}_3\text{-Al-O})$ unit, in order to calculate the molar quantities of MAO used in the preparation of the catalysts described in the examples below. Similarly the molar mass of ethylaluminosilane (EAO) was taken as 72.042 g/mol, corresponding to the $(\text{CH}_3\text{CH}_2\text{-Al-O})$ building block, and that of modified methylaluminosilane prepared from a 70:30 mixture of trimethylaluminium and triisobutylaluminium as 70.7 g/mol corresponding to the $(\text{Me}_{0.70}\text{isobu}_{0.30}\text{-Al-O})$ unit. Ethylene oligomerisation products were analysed by GC-MS and GC-FID.

The mixed heteroatomic PNP ligands were made by reacting amines and phosphine chlorides R_2PCl as described in (a) Ewart *et al*, *J. Chem. Soc.* **1964**, 1543; (b) Dossett, S.J. *et al*, *Chem. Commun.*, **2001**, 8, 699; (c) Balakrishna, M.S. *et al*, *J. Organomet. Chem.* **1990**, 390, 2, 203). The respective phosphine chlorides R_2PCl were prepared as described in literature (Casalnuovo, A.L. *et al*, *J. Am. Chem. Soc.* **1994**, 116, 22, 9869; Rajanbabu, T.V. *et al*, *J. Org. Chem.* **1997**, 62, 17, 6012).

Example 1 : Preparation of the (4-methoxyphenyl)₂PN(isopropyl)P(4-phenyl)₂ ligand

Example 1a) : Preparation of N,N-Diisopropylphosphoramidate dichloride

Diisopropylamine (70 ml, 0.50 mol) in toluene (80 ml) was added to a solution of PCl₃ (21.87 ml, 0.25 mol) in toluene (80 ml) at -10 °C. The mixture was stirred for two hours and then allowed to warm to room temperature. The solution was stirred for a further hour after which it was filtered through a pad of celite. The product (35 g, 0.17 mol, 68 %) was obtained after removal of the solvent. ³¹P {H} NMR: 170 ppm

Example 1b) Preparation of 4-methoxyphenyl-magnesium bromide

Magnesium turnings (9.11 g, 0.375 mol) were treated with 4-bromoanisole (9.39 ml, 75 mmol) in THF (100 ml). A vigorous reaction ensued which was cooled in an ice bath. Once the reaction had dissipated, the reaction mixture was heated under reflux for 2 hours yielding the Grignard reagent.

Example 1c) : Preparation of Bis(4-methoxyphenyl) phosphorus chloride

The Grignard reagent was added to N,N-diisopropylphosphoramidate dichloride (6.64 ml, 36 mmol) in THF (100 ml) at 0 °C. After stirring at room temperature overnight the mixture was diluted with cyclohexane (200 ml) and dry HCl gas was bubbled through the solution for 0.5 hours. After filtration of the precipitate, the solvent was removed to give a mixture of the phosphine chloride and bromide in an 80% yield. This crude product was not isolated and all was used in the next step.

Example 1d) : Preparation of (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂

To a solution of the crude Bis(4-methoxyphenyl) phosphorus chloride (28.8 mmol calculated from crude reaction mixture) in DCM (80 ml) and triethylamine (15 ml) at 0 °C was added isopropylamine (1.11 ml, 13 mmol). The reaction was stirred for 30 min after

which the ice bath was removed. After stirring for a total of 14 hrs the solution was filtered to remove the triethylammonium salt formed. The product was isolated after crystallisation in a 77 % yield. ^{31}P {H} NMR: 47.4 ppm (broad singlet)

Example 2: Ethylene tetramerisation reaction using Cr (III) acetylacetonate, (4-methoxyphenyl) $_2$ PN(methyl)P(4-methoxyphenyl) $_2$ and MAO

A solution of 30.0 mg of (4-methoxyphenyl) $_2$ PN(methyl)P(4-methoxyphenyl) $_2$ (0.066 mmol) in 10 ml of toluene was added to a solution of 11.5 mg chromium (III) acetylacetonate (0.033 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of toluene (80ml) and MAO (methylaluminoxane, 9.9 mmol) at 60°C. The pressure reactor was charged with ethylene after which the reactor temperature was maintained at 65°C, while the ethylene pressure was kept at 30 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after 30 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 0.2254 g of polyethylene. The GC analyses indicated that the reaction mixture contained 38.50g oligomers. The product distribution of this example is summarised in Table 1.

Example 3: Ethylene tetramerisation reaction using Cr (III) acetylacetonate, (3-methoxyphenyl) $_2$ PN(methyl)P(3-methoxyphenyl) $_2$ and MAO

A solution of 30.0 mg of (3-methoxyphenyl) $_2$ PN(methyl)P(3-methoxyphenyl) $_2$ (0.066 mmol) in 10 ml of toluene was added to a solution of 11.5 mg chromium (III) acetylacetonate (0.033 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of toluene (80ml) and MAO

(methylaluminoxane, 9.9 mmol) at 60°C. The pressure reactor was charged with ethylene after which the reactor temperature was maintained at 65°C, while the ethylene pressure was kept at 30 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after 30 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 1.2269 g of polyethylene. The GC analyses indicated that the reaction mixture contained 9.71g oligomers. The product distribution of this example is summarised in Table 1.

Example 4: Ethylene tetramerisation reaction using Cr (III) acetylacetonate, (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ and MAO

A solution of 36.1 mg of (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ (0.066 mmol) in 10 ml of toluene was added to a solution of 11.5 mg chromium (III) acetylacetonate (0.033 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of toluene (80ml) and MAO (methylaluminoxane, 9.9 mmol) at 60°C. The pressure reactor was charged with ethylene after which the reactor temperature was maintained at 65°C, while the ethylene pressure was kept at 30 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after 30 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 0.7105 g of polyethylene. The GC analyses indicated

that the reaction mixture contained 61.33g oligomers. The product distribution of this example is summarised in Table 1.

Example 5: Ethylene tetramerisation reaction using Cr (III) acetylacetonate, (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ and MAO

A solution of 36.1 mg of (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ (0.066 mmol) in 10 ml of toluene was added to a solution of 11.5 mg chromium (III) acetylacetonate (0.033 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor, (autoclave) containing a mixture of toluene (80ml) and MAO (methylaluminoxane, 9.9 mmol) at 40°C. The pressure reactor was charged with ethylene after which the reactor temperature was maintained at 45°C, while the ethylene pressure was kept at 45 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after 12 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 2.3010 g of polyethylene. The GC analyses indicated that the reaction mixture contained 73.53g oligomers. The product distribution of this example is summarised in Table 1.

Example 6: Ethylene tetramerisation reaction using Cr (III) acetylacetonate, (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ and MAO

A solution of 16.4 mg of (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ (0.03 mmol) in 10 ml of cyclohexane was added to a solution of 5.2 mg chromium (III) acetylacetonate (0.015 mmol) in 10 ml cyclohexane in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of cyclohexane (80ml) and MAO (methylaluminoxane in toluene, 4.5 mmol) at 40°C. The pressure reactor was charged with ethylene after which the reactor temperature was maintained at 45°C, while the

ethylene pressure was kept at 45 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after 11 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 1.9168 g of polyethylene. The GC analyses indicated that the reaction mixture contained 62.72g oligomers. The product distribution of this example is summarised in Table 1.

Example 7: Ethylene tetramerisation reaction using Cr (III) acetylacetonate, (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ and MAO

A solution of 9.8 mg of (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ (0.018 mmol) in 10 ml of toluene was added to a solution of 5.2 mg chromium (III) acetylacetonate (0.015 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of toluene (80ml) and MAO (methylaluminoxane, 4.5 mmol) at 40°C. The pressure reactor was charged with ethylene after which the reactor temperature was maintained at 45°C, while the ethylene pressure was kept at 45 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after 21 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 0.8280 g of polyethylene. The GC analyses indicated that the reaction mixture contained 69.17 g oligomers. The product distribution of this example is summarised in Table 1.

Example 8: Ethylene tetramerisation reaction using $\text{CrCl}_3 \cdot \text{THF}_3$, (4-methoxyphenyl) $_2\text{PN}(\text{isopropyl})\text{P}(\text{4-methoxyphenyl})_2$ and MAO

A solution of 9.8 mg of (4-methoxyphenyl) $_2\text{PN}(\text{isopropyl})\text{P}(\text{4-methoxyphenyl})_2$ (0.018 mmol) in 10 ml of toluene was added to a solution of 5.6 mg $\text{CrCl}_3 \cdot \text{THF}_3$ (0.015 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of toluene (80ml) and MAO (methylaluminoxane, 4.5 mmol) at 40°C. The pressure reactor was charged with ethylene after which the reactor temperature was maintained at 45°C, while the ethylene pressure was kept at 45 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after 30 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 1.0831 g of polyethylene. The GC analyses indicated that the reaction mixture contained 42.72 g oligomers. The product distribution of this example is summarised in Table 1.

Example 9: Ethylene tetramerisation reaction using Cr (III) 2-ethylhexanoate , (4-methoxyphenyl) $_2\text{PN}(\text{isopropyl})\text{P}(\text{4-methoxyphenyl})_2$ and MAO

A solution of 9.8 mg of (4-methoxyphenyl) $_2\text{PN}(\text{isopropyl})\text{P}(\text{4-methoxyphenyl})_2$ (0.018 mmol) in 10 ml of toluene was added to a solution of 10.2 mg Cr (III) 2-ethylhexanoate (70% in mineral oil, 0.015 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of toluene (80ml) and MAO (methylaluminoxane, 4.5 mmol) at 40°C. The pressure reactor was charged with ethylene after which the reactor temperature was maintained at 45°C, while the ethylene pressure was kept at 45 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after

30 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 1.52 g of polyethylene. The GC analyses indicated that the reaction mixture contained 61.27 g oligomers. The product distribution of this example is summarised in Table 1.

Example 10: Ethylene tetramerisation reaction using Cr (III) octanoate , (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ and MAO

A solution of 9.8 mg of (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ (0.018 mmol) in 10 ml of toluene was added to a solution of 10.3 mg Cr (III) octanoate (70% in toluene, 0.015 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of toluene (80ml) and MAO (methylaluminoxane, 4.5 mmol) at 40°C. The pressure reactor was charged with ethylene after which the reactor temperature was maintained at 45°C, while the ethylene pressure was kept at 45 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after 40 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 0.3773 g of polyethylene. The GC analyses indicated that the reaction mixture contained 18.91 g oligomers. The product distribution of this example is summarised in Table 1.

Example 11: Ethylene tetramerisation reaction using Cr (III) acetylacetonate, (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ and MAO

A solution of 6.6 mg of (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ (0.012 mmol) in 10 ml of toluene was added to a solution of 3.5 mg chromium (III) acetylacetonate (0.015 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of toluene (80ml) and MAO (methylaluminoxane, 3.0 mmol) at 40°C. The pressure reactor was charged with ethylene after which the reactor temperature was maintained at 45°C, while the ethylene pressure was kept at 45 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after 30 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 1.3958 g of polyethylene. The GC analyses indicated that the reaction mixture contained 54.52 g oligomers. The product distribution of this example is summarised in Table 1.

Example 12: Ethylene tetramerisation reaction using Cr (III) acetylacetonate, (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ and MAO

A solution of 9.8 mg of (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ (0.018 mmol) in 10 ml of toluene was added to a solution of 5.2 mg chromium (III) acetylacetonate (0.015 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of toluene (80ml) and MAO (methylaluminoxane in toluene, 2.25 mmol) at 40°C. The pressure reactor was charged with ethylene after which the reactor temperature was maintained at 45°C, while the ethylene pressure was kept at 45 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after 15 minutes by

discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 0.5010 g of polyethylene. The GC analyses indicated that the reaction mixture contained 70.87 g oligomers. The product distribution of this example is summarised in Table 1.

Example 13: Ethylene tetramerisation reaction using Cr (III) acetylacetonate, (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ and MMAO-3A

A solution of 16.4 mg of (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ (0.03 mmol) in 10 ml of toluene was added to a solution of 5.2 mg chromium (III) acetylacetonate (0.015 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of toluene (80ml) and MMAO-3A (modified methylaluminoxane in heptanes, 4.5 mmol) at 40°C. The pressure reactor was charged with ethylene after which the reactor temperature was maintained at 45°C, while the ethylene pressure was kept at 45 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after 22 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 1.76 g of polyethylene. The GC analyses indicated that the reaction mixture contained 50.42g oligomers. The product distribution of this example is summarised in Table 1.

Example 14: Ethylene tetramerisation reaction using Cr (III) acetylacetonate, (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ and EAO/TMA

A solution of 36.1 mg of (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ (0.066 mmol) in 10 ml of toluene was added to a solution of 5.2 mg chromium (III) acetylacetonate (0.015 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of toluene (80ml), EAO (ethylaluminumoxane in toluene, 33 mmol) and TMA (trimethylaluminium, 8.25mmol) at 40°C. The pressure reactor was charged with ethylene after which the reactor temperature was maintained at 45°C, while the ethylene pressure was kept at 45 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after 60 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 0.189 g of polyethylene. The GC analyses indicated that the reaction mixture contained 40.97g oligomers. The product distribution of this example is summarised in Table 1.

Example 15: Ethylene tetramerisation reaction using Cr (III) acetylacetonate, (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ and MAO in the presence of H₂

A solution of 16.4 mg of (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂ (0.03 mmol) in 10 ml of toluene was added to a solution of 5.2 mg chromium (III) acetylacetonate (0.015 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of toluene (80ml) and MAO (methylaluminumoxane in toluene, 4.5 mmol) at 40°C. The pressure reactor was first charged with hydrogen to a pressure of approximately 2.5 barg and subsequently with ethylene to 45 barg after which the reactor temperature was maintained at 45°C, while the ethylene pressure was kept at 45 barg. Thorough mixing was ensured throughout by mixing speeds of 1100

RPM's using a gas entraining stirrer. The reaction was terminated after 15 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 1.2060 g of polyethylene. The GC analyses indicated that the reaction mixture contained 81.51 g oligomers. The product distribution of this example is summarised in Table 1.

Example 16: Ethylene tetramerisation reaction using Cr (III) acetylacetonate, (phenyl)₂PN(isopropyl)P(2-methoxyphenyl)₂ and MAO

A solution of 32.2 mg of (phenyl)₂PN(isopropyl)P(2-methoxyphenyl)₂ (0.066 mmol) in 10 ml of toluene was added to a solution of 11.5 mg chromium (III) acetylacetonate (0.033 mmol) in 10 ml toluene in a Schlenk vessel. The mixture was stirred for 5 min at ambient temperature and was then transferred to a 300 ml pressure reactor (autoclave) containing a mixture of toluene (80ml) and MAO (methylaluminoxane in toluene, 4.5 mmol) at 40°C. The pressure reactor was first charged with ethylene after which the reactor temperature was maintained at 45°C, while the ethylene pressure was kept at 45 barg. Thorough mixing was ensured throughout by mixing speeds of 1100 RPM's using a gas entraining stirrer. The reaction was terminated after 15 minutes by discontinuing the ethylene feed to the reactor and cooling the reactor to below 10°C. After releasing the excess ethylene from the autoclave, the liquid contained in the autoclave was quenched with ethanol followed by 10% hydrochloric acid in water. Nonane was added as an internal standard for the analysis of the liquid phase by GC-FID. A small sample of the organic layer was dried over anhydrous sodium sulfate and then analysed by GC-FID. The remainder of the organic layer was filtered to isolate the solid wax/polymeric products. These solid products were dried overnight in an oven at 100°C and then weighed to yield 6.82 g of polyethylene. The GC analyses indicated that the reaction mixture contained 38.33 g oligomers. The product distribution of this example is summarised in Table 1.

Table 1: Ethylene tetramerisation runs: Examples 2- 16

Example	Activity	Total Product	Solids	Liquids	Liquid Product Distribution					1-Octene in C ₈
	g prod./g Cr	g	Wt %	Wt %	Wt %					Wt %
					C ₄	C ₆	C ₈	C ₁₀	C ₁₁₊	
2	22622	38.72	0.58	99.42	3.2	26.0	50.1	4.2	16.0	93.5
3	6376	10.94	11.21	88.79	2.8	33.8	37.5	1.4	19.5	92.2
4	36156	62.04	1.15	98.08	0.5	39.1	51.5	2.9	5.8	98.8
5	44301	75.83	3.03	96.97	1.2	24.4	61.1	1.0	10.7	98.0
6	83515	62.64	2.97	97.03	1.0	24.5	54.9	1.0	16.0	97.0
7	90432	69.99	1.18	98.82	1.1	23.2	62.9	0.6	10.9	98.4
8	56365	43.80	2.47	97.53	1.1	24.4	69.3	0.8	3.6	98.9
9	80510	62.79	2.42	97.58	1.3	23.1	62.7	2.6	10.1	98.0
10	24924	19.29	1.96	98.04	1.0	23.4	67.3	0.9	6.4	98.6
11	107331	55.92	2.50	97.50	1.3	25.4	63.0	1.0	7.8	98.0
12	92214	71.37	0.70	99.30	1.0	23.5	65.4	0.9	3.1	98.6
13	66911	52.18	3.37	96.86	2.0	18.3	65.8	2.7	11.1	98.4
14	23987	41.16	0.46	99.54	2.1	28.3	63.5	1.4	4.5	98.2
15	106055	82.71	1.46	98.54	1.9	32.6	63.2	1.1	1.1	98.0
16	26310	45.15	15.11	84.89	0.3	36.7	46.3	5.8	10.6	98.5

Claims

1. A process for tetramerisation of olefins wherein the product stream of the process contains more than 30% of the tetramer olefin.
2. A process as claimed in Claim 1 which process includes the step of contacting an olefinic feedstream with a catalyst system containing a transition metal compound and a heteroatomic ligand.
3. A process as claimed in Claim 1 or Claim 2, wherein the heteroatomic ligand is described by the following general formula $(R)_nA-B-C(R)_m$ where A and C are independently selected from a group which comprises phosphorus, arsenic, antimony, oxygen, bismuth, sulphur, selenium, and nitrogen, and B is a linking group between A and C, and the R's are the same or different and each R is independently selected from any homo or hetero hydrocarbonyl group and n and m for each R is independently determined by the respective valence and oxidation state of A and C and of which at least one of the R's is substituted with a polar substituent.
4. A process as claimed in Claim 3, wherein the ligand comprises of multiples of $(R)_nA-B-C(R)_m$.
5. A process as claimed in any one of claims 1 to 3, which process includes the step of contacting an olefinic feedstream with a catalyst system which includes a transition metal and a heteroatomic ligand and wherein the tetramer is an olefin and makes up more than 30% of the product stream of the process and wherein the heteroatomic ligand is described by the following general formula $(R^1)(R^2)A-B-C(R^3)(R^4)$ where A and C are independently selected from a group which comprises phosphorus, arsenic, antimony, bismuth, and nitrogen and B is a linking group between A and C, and R^1 , R^2 , R^3 and R^4 are independently selected from non-aromatic and aromatic, including heteroaromatic, groups of which at least one of R^1 , R^2 , R^3 and R^4 is substituted with a polar substituent.

6. A process as claimed in Claim 5, wherein up to four of R¹, R², R³ and R⁴ have substituents on the atom adjacent to the atom bound to A or C.
7. A process as claimed in Claim 5 or Claim 6, wherein each of R¹, R², R³ and R⁴ is aromatic, including heteroaromatic, but not all of R¹, R², R³ and R⁴ are substituted by any substituent on an atom adjacent to the atom bound to A or C.
8. A process as claimed in Claim 7, wherein not more than two of R¹, R², R³ and R⁴ have substituents on the atom adjacent to the atom bound to A or C.
9. A process as claimed in Claim 7 or Claim 8, wherein any polar substituents on R¹, R², R³ and R⁴ are not on the atom adjacent to the atom bound to A or C.
10. A process as claimed in any one of claims 5 and 7 to 9, wherein at least one of R¹, R², R³ and R⁴ is substituted with a polar substituent on the 2nd or further atom from the atom bound to A or C.
11. A process as claimed in any one of claims 3 to 5 and 7 to 10, wherein any polar substituents on one or more of R¹, R², R³ and R⁴ are electron donating.
12. A process as claimed in any one of claims 1 to 5 and 7 to 11, wherein the feedstream includes an α -olefin and the product stream includes at least 30% of a tetramerised α -olefin monomer.
13. A process as claimed in any one of claims 1 to 5 and 7 to 12, wherein the olefinic feedstream includes ethylene and the product stream includes at least 30% 1-octene.
14. A process as claimed in any one of claims 1 to 5 and 7 to 12, wherein the olefinic feedstream includes ethylene and the product stream includes at least 40% 1-octene.
15. A process as claimed in any one of claims 1 to 5 and 7 to 12, wherein the olefinic feedstream includes ethylene and the product stream includes at least 50% 1-octene.

16. A process as claimed in any one of claims 1 to 5 and 7 to 12, wherein the olefinic feedstream includes ethylene and the product stream includes at least 60% 1-octene.
17. A process as claimed in any one of claims 1 to 5 and 7 to 16, wherein the olefinic feedstream includes ethylene and wherein the $(C_6 + C_8) : (C_4 + C_{10})$ ratio in the product stream is more than 2.5:1.
18. A process as claimed in any one of claims 1 to 5 and 7 to 17, wherein the olefinic feedstream includes ethylene and wherein the $C_8 : C_6$ ratio in the product stream is more than 1.
19. A process as claimed in any one of claims 12 to 18, wherein ethylene is contacted with the catalyst system at a pressure of more than 10 barg.
20. A process as claimed in any one of claims 3 to 5 and 7 to 19, wherein A and/or C are a potential electron donor for coordination with the transition metal.
21. A process as claimed in any one of claims 3 to 5 and 7 to 20, wherein B is selected from any one of a group comprising: organic linking groups comprising a hydrocarbyl, substituted hydrocarbyl, heterohydrocarbyl and a substituted heterohydrocarbyl; inorganic linking groups comprising single atom links; ionic links; and a group comprising methylene, dimethylmethylene, 1,2-ethane, 1,2-phenylene, 1,2-propane, 1,2-catechol, 1,2-dimethylhydrazine, $-B(R^5)-$, $-Si(R^5)_2-$, $-P(R^5)-$ and $-N(R^5)-$ where R^5 is hydrogen, a hydrocarbyl or substituted hydrocarbyl, a substituted heteroatom and a halogen.
22. A process as claimed in any one of claims 3 to 5 and 7 to 21, wherein B is selected to be a single atom spacer.
23. A process as claimed in any one of claims 3 to 5 and 7 to 22, wherein B is selected to be $-N(R^5)-$, wherein R^5 is hydrogen or selected from the groups consisting of alkyl, substituted alkyl, aryl, substituted aryl, aryloxy, substituted aryloxy, halogen, nitro, alkoxycarbonyl, carbonyloxy, alkoxy, aminocarbonyl, carbonylamino, dialkylamino, silyl groups or derivatives thereof, and aryl substituted with any of these substituents.

24. A process as claimed in any one of claims 3 to 5 and 7 to 23, wherein A and/or C is independently oxidised by S, Se, N or O, where the valence of A and/or C allows for such oxidation.

25. A process as claimed in any one of claims 3 to 5 and 7 to 24, wherein A and C is independently phosphorous or phosphorous oxidised by S or Se or N or O.

26. A process as claimed in any one of claims 3 to 5 and 7 to 25, wherein R^1 , R^2 , R^3 and R^4 are independently selected from a group comprising a benzyl, phenyl, tolyl, xylyl, mesityl, biphenyl, naphthyl, anthracenyl, methoxy, ethoxy, phenoxy, tolyloxy, dimethylamino, diethylamino, methylethylamino, thiophenyl, pyridyl, thioethyl, thiophenoxy, trimethylsilyl, dimethylhydrazyl, methyl, ethyl, ethenyl, propyl, butyl, propenyl, propynyl, cyclopentyl, cyclohexyl, ferrocenyl and tetrahydrofuranyl group.

27. A process as claimed in any one of claims 3 to 5 and 7 to 26, wherein R^1 , R^2 , R^3 and R^4 are independently selected from a group comprising a phenyl, tolyl, biphenyl, naphthyl, thiophenyl and ethyl group.

28. A process as claimed in any one of claims 2 to 5, 7 to 23 and 25 to 27 wherein the ligand is selected from any one of a group comprising (3-methoxyphenyl)₂PN(methyl)P(3-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(methyl)P(4-methoxyphenyl)₂, (3-methoxyphenyl)₂PN(isopropyl)P(3-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(2-ethylhexyl)P(4-methoxyphenyl)₂, (3-methoxyphenyl)(phenyl)PN(methyl)P(phenyl)₂ and (4-methoxyphenyl)(phenyl)PN(methyl)P(phenyl)₂, (3-methoxyphenyl)(phenyl)PN(methyl)P(3-methoxyphenyl)(phenyl), (4-methoxyphenyl)(phenyl)PN(methyl)P(4-methoxyphenyl)(phenyl), (3-methoxyphenyl)₂PN(methyl)P(phenyl)₂ and (4-methoxyphenyl)₂PN(methyl)P(phenyl)₂, (4-methoxyphenyl)₂PN(1-cyclohexylethyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(2-methylcyclohexyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(decyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(pentyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(benzyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(phenyl)P(4-methoxyphenyl)₂, (4-fluorophenyl)₂PN(methyl)P(4-fluorophenyl)₂, (2-

fluorophenyl)₂PN(methyl)P(2-fluorophenyl)₂, (4-dimethylamino-phenyl)₂PN(methyl)P(4-dimethylamino-phenyl)₂, (4-methoxyphenyl)₂PN(allyl)P(4-methoxyphenyl)₂, (phenyl)₂PN(isopropyl)P(2-methoxyphenyl)₂, (4-(4-methoxyphenyl)-phenyl)₂PN(isopropyl)P(4-(4-methoxyphenyl)-phenyl)₂ and (4-methoxyphenyl)(phenyl)PN(isopropyl)P(phenyl)₂.

29. A process as claimed in any one of the claims 1 to 5 and 7 to 28, which process includes the step of combining in any order a heteroatomic ligand with a transition metal compound and an activator.

30. A process as claimed in any one of claims 2 to 5 and 7 to 28, which process includes the step of adding a pre-formed coordination complex, prepared using the heteroatomic ligand and a transition metal compound, to a reaction mixture containing an activator,

31. A process as claimed in Claim 30, which includes the step of generating a heteroatomic coordination complex *in situ* from a transition metal compound and a heteroatomic ligand.

32. A process as claimed in any one of the claims 2 to 5 and 7 to 31, wherein the transition metal is selected from any one of a group comprising chromium, molybdenum, tungsten, titanium, tantalum, vanadium and zirconium.

33. A process as claimed in any one of the claims 2 to 5 and 7 to 32, wherein the transition metal is chromium.

34. A process as claimed in any one of claims 29 to 31, wherein the transition metal compound is selected from a group comprising of an inorganic salt, organic salt, a coordination complex and organometallic complex.

35. A process as claimed in Claim 34, wherein the transition metal compound is selected from any one of a group comprising chromium trichloride tris-tetrahydrofuran complex, (benzene)tricarbonyl chromium, chromium (III) octanoate, chromium (III) acetylacetonate, chromium hexacarbonyl and chromium (III) 2-ethylhexanoate.

36. A process as claimed in any one of claims 29 to 31 and 33 to 35, wherein the transition metal compound is selected from a complex selected from chromium (III) acetylacetonate and chromium (III) 2-ethylhexanoate.

37. A process as claimed in any one of claims 29 to 36, wherein the transition metal from a transition metal compound and heteroatomic ligand are combined to provide metal/ligand ratios from about 0.01:100 to 10 000:1.

38. A process as claimed in Claim 37, wherein the transition metal compound and heteroatomic ligand are combined to provide metal/ligand ratios from about 0.1:1 to 10:1.

39. A process as claimed in any one of claims 29 to 38, wherein the catalyst system includes an activator selected from any one of a group consisting of organoaluminium compounds, organoboron compounds, organic salts, such as methyllithium and methylmagnesium bromide, inorganic acids and salts, such as tetrafluoroboric acid etherate, silver tetrafluoroborate and sodium hexafluoroantimonate.

40. A process as claimed in any one of claims 29 to 31, wherein the activator is selected from alkylaluminoxanes.

41. A process as claimed in Claim 40, wherein the alkylaluminoxane, or mixtures thereof, is selected from group which consists of methylaluminoxane (MAO), ethylaluminoxane (EAO) and modified alkylaluminoxanes (MMAO).

42. A process as claimed in Claim 41, wherein the transition metal and the aluminoxane are combined in proportions to provide Al/metal ratios from about 1:1 to 10 000:1.

43. A process as claimed in Claim 42, wherein the transition metal and the aluminoxane are combined in proportions to provide Al/metal ratios from about 1:1 to 1000:1.

44. A process as claimed in Claim 43, wherein the transition metal and the aluminoxane are combined in proportions to provide Al/metal ratios from about 1:1 to 300:1.

45. A process as claimed in any one of claims 42 to 44, which includes the step of adding to the catalyst system a trialkylaluminium compound in amounts of between 0.01 to 100 mol per mol of alkylaluminoxane.

46. A process as claimed in any one of claims 2 to 5 and 7 to 45, which includes the step of mixing the components of the catalyst system at any temperature between -20°C and 250°C in the presence of an olefin.

47. A process as claimed in any one of claims 2 to 5 and 7 to 46, wherein the product stream is contacted with the catalyst system at a temperature ranging between 15 and 130 °C.

48. A process as claimed in claims 1 to 5 and 7 to 47, wherein methylcyclopentane and methylene cyclopentane are formed as products and independently make up at least 1% of the product stream of the process.

49. A tetramerisation catalyst system which includes a transition metal and a heteroatomic ligand described by the following general formula $(R)_nA-B-C(R)_m$ where A and C are independently selected from a group which comprises phosphorus, arsenic, antimony, oxygen, bismuth, sulphur, selenium, and nitrogen, and B is a linking group between A and C, and the R's are the same or different and each R is independently selected from any homo or hetero hydrocarbonyl group and n and m for each R is independently determined by the respective valence and oxidation state of A and C and of which at least one of the R's is substituted with a polar substituent.

50. A catalyst system as claimed in Claim 49, wherein the ligand comprises of multiples of $(R)_nA-B-C(R)_m$.

51. A catalyst system as claimed in Claim 49 or Claim 50 which includes a transition metal and a heteroatomic ligand described by the following general formula $(R^1)(R^2)A-B-$

$C(R^3)(R^4)$ where A and C are independently selected from a group which comprises phosphorus, arsenic, antimony, bismuth, and nitrogen and B is a linking group between A and C, and R^1 , R^2 , R^3 and R^4 are independently selected from non-aromatic and aromatic, including heteroaromatic, groups of which at least one of R^1 , R^2 , R^3 and R^4 is substituted with a polar substituent.

52. A catalyst system as claimed in Claim 50 or Claim 51, wherein each of R^1 , R^2 , R^3 and R^4 is aromatic, including heteroaromatic, but not all of R^1 , R^2 , R^3 and R^4 are substituted by any substituent on an atom adjacent to the atom bound to A or C.

53. A catalyst system as claimed in Claim 51 or Claim 52, wherein not more than two of R^1 , R^2 , R^3 and R^4 have substituents on the atom adjacent to the atom bound to A or C.

54. A catalyst system as claimed in Claim 52, wherein any polar substituents on R^1 , R^2 , R^3 and R^4 are not on the atom adjacent to the atom bound to A or C.

55. A catalyst system as claimed in any one of claims 52 to 54, wherein at least one of R^1 , R^2 , R^3 and R^4 is substituted with a polar substituent on the 2nd or further atom from the atom bound to A or C.

56. A catalyst system as claimed in any one of claims 49 to 55, wherein any polar substituents on one or more of R^1 , R^2 , R^3 and R^4 are electron donating.

57. A catalyst system as claimed in any one of claims 49 to 56, wherein A and/or C are a potential electron donor for coordination with the transition metal.

58. A catalyst system as claimed in any one of claims 49 to 57, wherein B is selected from any one of a group comprising: organic linking groups comprising a hydrocarbyl, substituted hydrocarbyl, heterohydrocarbyl and a substituted heterohydrocarbyl; inorganic linking groups comprising single atom links; ionic links; and a group comprising methylene, dimethylmethylene, 1,2-ethane, 1,2-phenylene, 1,2-propane, 1,2-catechol, 1,2-dimethylhydrazine, $-B(R^5)-$, $-Si(R^5)_2-$, $-P(R^5)-$ and $-N(R^5)-$ where R^5 is hydrogen, a hydrocarbyl or substituted hydrocarbyl, a substituted heteroatom and a halogen.

59. A catalyst system as claimed in any one of claims 49 to 58, wherein B is selected to be a single atom spacer.

60. A catalyst system as claimed in any one of claims 49 to 59, wherein B is selected to be $-N(R^5)-$, wherein R^5 is hydrogen or selected from the groups consisting of alkyl, substituted alkyl, aryl, substituted aryl, aryloxy, substituted aryloxy, halogen, nitro, alkoxycarbonyl, carbonyloxy, alkoxy, aminocarbonyl, carbonylamino, dialkylamino, silyl groups or derivatives thereof, and aryl substituted with any of these substituents.

61. A catalyst system as claimed in any one of claims 50 to 60, wherein A and/or C is independently oxidised by S, Se, N or O, where the valence of A and/or C allows for such oxidation.

62. A catalyst system as claimed in any one of claims 50 to 60, wherein A and C is independently phosphorus or phosphorus oxidised by S or Se or N or O.

63. A catalyst system as claimed in any one of claims 49 to 62, wherein R^1 , R^2 , R^3 and R^4 are independently selected from a group comprising a benzyl, phenyl, tolyl, xylyl, mesityl, biphenyl, naphthyl, anthracenyl, methoxy, ethoxy, phenoxy, tolyloxy, dimethylamino, diethylamino, methylethylamino, thiophenyl, pyridyl, thioethyl, thiophenoxy, trimethylsilyl, dimethylhydrazyl, methyl, ethyl, ethenyl, propyl, butyl, propenyl, propynyl, cyclopentyl, cyclohexyl, ferrocenyl and tetrahydrofuranyl group.

64. A catalyst system as claimed in any one of claims 49 to 63, wherein R^1 , R^2 , R^3 and R^4 are independently selected from a group comprising a phenyl, tolyl, biphenyl, naphthyl, thiophenyl and ethyl group.

65. A catalyst system as claimed in any one of claims 50 to 60 and 62 to 64 wherein the ligand is selected from any one of a group comprising (3-methoxyphenyl)₂PN(methyl)P(3-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(methyl)P(4-methoxyphenyl)₂, (3-methoxyphenyl)₂PN(isopropyl)P(3-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(isopropyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(2-ethylhexyl)P(4-methoxyphenyl)₂, (3-methoxyphenyl)(phenyl)PN(methyl)P(phenyl)₂ and (4-methoxyphenyl)(phenyl)PN(methyl)P(phenyl)₂, (3-

methoxyphenyl)(phenyl)PN(methyl)P(3-methoxyphenyl)(phenyl), (4-methoxyphenyl)(phenyl)PN(methyl)P(4-methoxyphenyl)(phenyl), (3-methoxyphenyl)₂PN(methyl)P(phenyl)₂ and (4-methoxyphenyl)₂PN(methyl)P(phenyl)₂, (4-methoxyphenyl)₂PN(1-cyclohexylethyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(2-methylcyclohexyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(decyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(pentyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(benzyl)P(4-methoxyphenyl)₂, (4-methoxyphenyl)₂PN(phenyl)P(4-methoxyphenyl)₂, (4-fluorophenyl)₂PN(methyl)P(4-fluorophenyl)₂, (2-fluorophenyl)₂PN(methyl)P(2-fluorophenyl)₂, (4-dimethylamino-phenyl)₂PN(methyl)P(4-dimethylamino-phenyl)₂, (4-methoxyphenyl)₂PN(allyl)P(4-methoxyphenyl)₂, (phenyl)₂PN(isopropyl)P(2-methoxyphenyl)₂, (4-(4-methoxyphenyl)-phenyl)₂PN(isopropyl)P(4-(4-methoxyphenyl)-phenyl)₂ and (4-methoxyphenyl)(phenyl)PN(isopropyl)P(phenyl)₂.

66. A catalyst system as claimed any one of the claims 49 to 65, wherein the transition metal is selected from any one of a group comprising chromium, molybdenum, tungsten, titanium, tantalum, vanadium and zirconium.

67. A catalyst system as claimed in any one of the claims 49 to 66, wherein the transition metal is chromium.

68. A catalyst system as claimed in Claim 67, wherein the transition metal is derived from a transition metal compound selected from a group comprising of an inorganic salt, organic salt, a co-ordination complex and organometallic complex.

69. A catalyst system as claimed in Claim 68, wherein the transition metal compound is selected from a group comprising chromium trichloride tris-tetrahydrofuran complex, (benzene)tricarbonyl chromium, chromium (III) octanoate, chromium (III) acetylacetonate, chromium hexacarbonyl, and chromium (III) 2-ethylhexanoate.

70. A catalyst system as claimed in any one of claims 49 to 69, wherein the transition metal is selected from a complex selected from chromium (III) acetylacetonate and chromium (III) 2-ethylhexanoate.

71. A catalyst system as claimed in Claim 68 or Claim 69, wherein the transition metal from a transition metal compound and heteroatomic ligand are combined to provide metal/ligand ratios from about 0.01:100 to 10 000:1.
72. A catalyst as claimed in Claim 71, wherein the transition metal compound and heteroatomic ligand are combined to provide metal/ligand ratios from about 0.1:1 to 10:1.
73. A catalyst system as claimed in any one of the claims 49 to 72, which includes an activator.
74. A catalyst system as claimed in Claim 73, wherein the activator is selected from any one of a group consisting of organoaluminium compounds, organoboron compounds, organic salts, such as methyllithium and methylmagnesium bromide, inorganic acids and salts, such as tetrafluoroboric acid etherate, silver tetrafluoroborate and sodium hexafluoroantimonate.
75. A catalyst system as claimed in Claim 73 or Claim 74, wherein the activator is selected from alkylaluminoxanes.
76. A catalyst system as claimed in Claim 75, wherein the alkylaluminoxane, or mixtures thereof, is selected from group which consists of methylaluminoxane (MAO), ethylaluminoxane (EAO) and modified alkylaluminoxanes (MMAO).
77. A catalyst system as claimed in Claim 75 or Claim 76, wherein the transition metal and the aluminoxane are combined in proportions to provide Al/metal ratios from about 1:1 to 10 000:1.
78. A catalyst system as claimed in Claim 77, wherein the transition metal and the aluminoxane are combined in proportions to provide Al/metal ratios from about 1:1 to 1000:1.

79. A catalyst system as claimed in Claim 78, wherein the transition metal and the aluminosilicate are combined in proportions to provide Al/metal ratios from about 1:1 to 300:1.
80. A catalyst system as claimed in any one of claims 75 to 79, which includes a trialkylaluminum compound in amounts of between 0.01 to 100 mol per mol of aluminosilicate.
81. Use of a tetramerisation catalyst system as claimed in any one of claims 49 to 80 for the tetramerisation of olefins.
82. Use of a tetramerisation catalyst system as claimed in any one of claims 49 to 80 for the tetramerisation of ethylene.
83. Use of a ligand for a tetramerisation process as claimed in any one of claims 1 to 5 and 7 to 48.
84. Use of a ligand for a tetramerisation catalyst system as claimed in any one of claims 49 to 80.
83. An olefin tetramerisation process substantially as described herein.
84. An olefin tetramerisation catalyst system substantially as described herein.

INTERNATIONAL SEARCH REPORT

International Application No

PCT/ZA 03/00186

A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 B01J31/18 B01J31/24 C07C2/36 C07C11/02 C07C2/32

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 B01J C07C

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, WPI Data

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	<p>ANTHEA CARTER, STEVEN COHEN, NEIL COOLEY, ADEN MURPHY, JAMES SCUTT, DUNAN WASS: "High activity ethylene trimerisation catalysts based on diphosphine ligands" CHEMICAL COMMUNICATION, vol. 2002, no. 8, 20 March 2002 (2002-03-20), pages 858-859, XP002277009 cited in the application * table 1, entry 15, compound 3</p>	1-84
X	<p>WO 02/04119 A (WASS DUNCAN FRANK ;BP CHEM INT LTD (GB)) 17 January 2002 (2002-01-17) cited in the application claim 18</p>	1-84

☒ Further documents are listed in the continuation of box C.

☒ Patent family members are listed in annex.

* Special categories of cited documents :

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"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)

"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

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"&" document member of the same patent family

Date of the actual completion of the international search

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03/05/2004

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INTERNATIONAL SEARCH REPORT

International Application No

PCT/ZA 03/00186

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category °	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	US 4 628 138 A (BARNETT KENNETH W ET AL) 9 December 1986 (1986-12-09) table 1, entry 1 ---	1
X	US 2 699 457 A (KARL ZIEGLER ET AL) 11 January 1955 (1955-01-11) example 3 -----	1

INTERNATIONAL SEARCH REPORT

Information on patent family members

International Application No

PCT/ZA 03/00186

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			WO 0204119 A1	17-01-2002
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			NO 20030108 A	13-02-2003
			SK 172003 A3	11-09-2003
			US 2003166456 A1	04-09-2003
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US 2699457	A	11-01-1955	NONE	